

## Low-temperature oxidation of volatile organic compounds by ozone on Mn-promoted W/Al<sub>2</sub>O<sub>3</sub>

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### *Catalyst preparation*

A sample containing 8 wt.% W was prepared by incipient wetness impregnation γ-Al<sub>2</sub>O<sub>3</sub> ("Sasol", S<sub>BET</sub> = 76 m<sup>2</sup> g<sup>-1</sup>) with an aqueous solution of (NH<sub>4</sub>)<sub>6</sub>W<sub>12</sub>O<sub>39</sub>·H<sub>2</sub>O, (Aldrich). A 1% Mn/Al<sub>2</sub>O<sub>3</sub> sample was prepared by impregnation with an aqueous solution of Mn(NO<sub>3</sub>)<sub>2</sub>·4H<sub>2</sub>O (≥97%, Sigma Aldrich, USA). A 1% Mn8%W/Al<sub>2</sub>O<sub>3</sub> sample was prepared by additional impregnation of a monolayer 8%W/Al<sub>2</sub>O<sub>3</sub> with an aqueous solution of Mn(NO<sub>3</sub>)<sub>2</sub>·4H<sub>2</sub>O (≥97%, Sigma Aldrich, USA). After impregnation, the samples were dried at room temperature and then calcined for 2 hours at 550°C.

### *Catalyst characterization*

**Temperature-programmed reduction (H<sub>2</sub>-TPR).** The catalysts were studied by temperature-programmed reduction by hydrogen on an USGA-101 semiautomatic flow setup (Unisit LLC, Russia) equipped with a catharometer calibrated against the reduction of NiO (99.99%, Sigma—Aldrich, USA). An U-shaped quartz reactor with a chromel—alumel thermocouple was loaded with a weighed sample of the catalyst (0.3 g). The sample was preliminarily purged with argon (99.999%, Linde Gas Rus PLC, Russia; flow rate 30 mL min<sup>-1</sup>) on heating from room temperature to 150°C at a rate of 10°C min<sup>-1</sup> and then allowed to stay at a specified temperature for 1 h. Then, the sample was cooled in Ar flow to 50°C and kept at a preset temperature in a 5%H<sub>2</sub>/Ar stream (Linde Gas Rus PLC, Russia) (30 mL min<sup>-1</sup>) until a stable baseline emerged (~20–30 min). The catalyst sample was reduced in a 5%H<sub>2</sub>/Ar flow (30 mL min<sup>-1</sup>) on heating to 650°C at a rate of 10°C min<sup>-1</sup>. To remove water vapor formed during the reduction reaction, a trap cooled to a temperature of –20°C with a Peltier element was placed between the reactor and the catharometer.

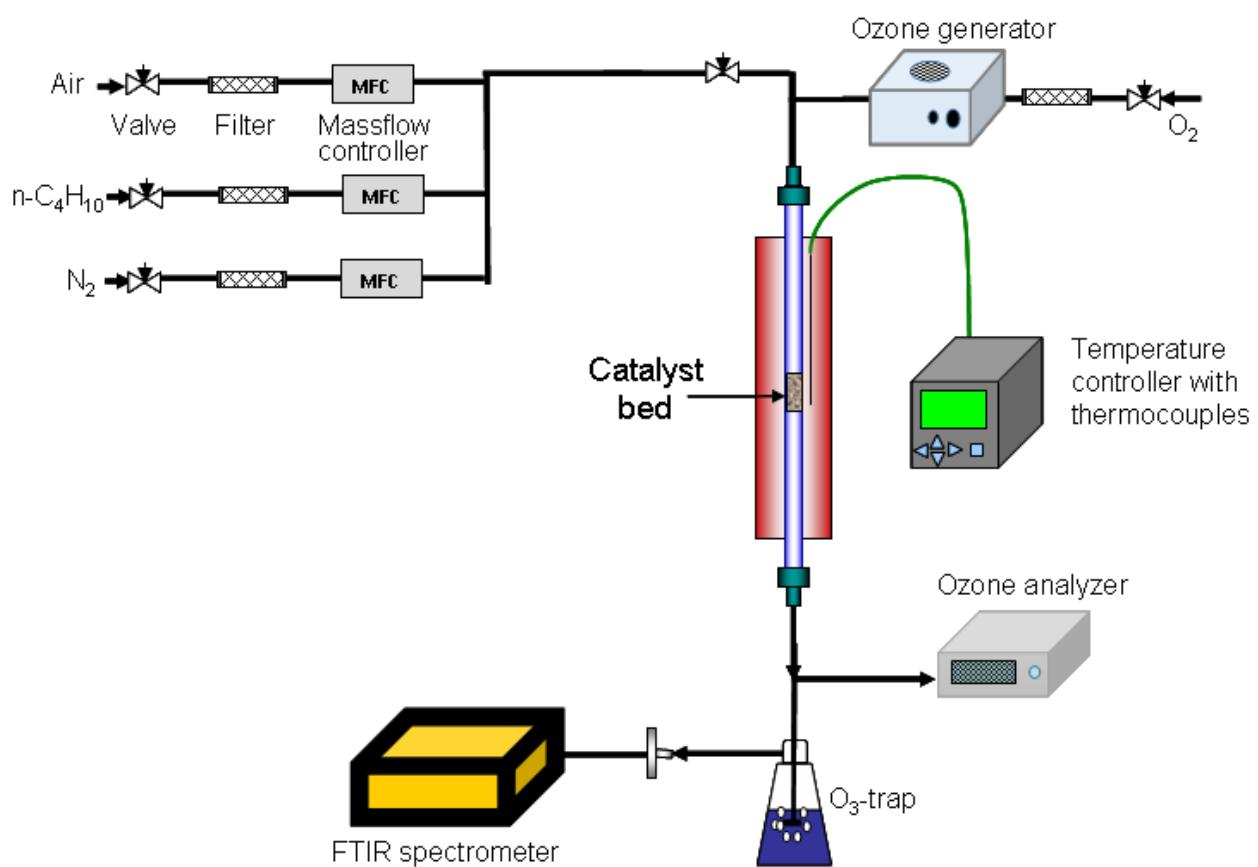
**Scanning electron microscopy (SEM-EDS)** The surface morphology of catalysts was characterized using SU8000 (Hitachi, Tokyo, Japan) field-emission scanning electron microscope (FE-SEM). Before measurements the samples were mounted on a 25 mm aluminum specimen stub and fixed by conductive graphite adhesive tape. Qualitative and quantitative analysis of catalyst elements were carried out using energy dispersive X-ray spectroscopy (EDS) on Oxford Instruments X-max 80 EDS system with 15 kV accelerating voltage.

#### *Catalytic tests*

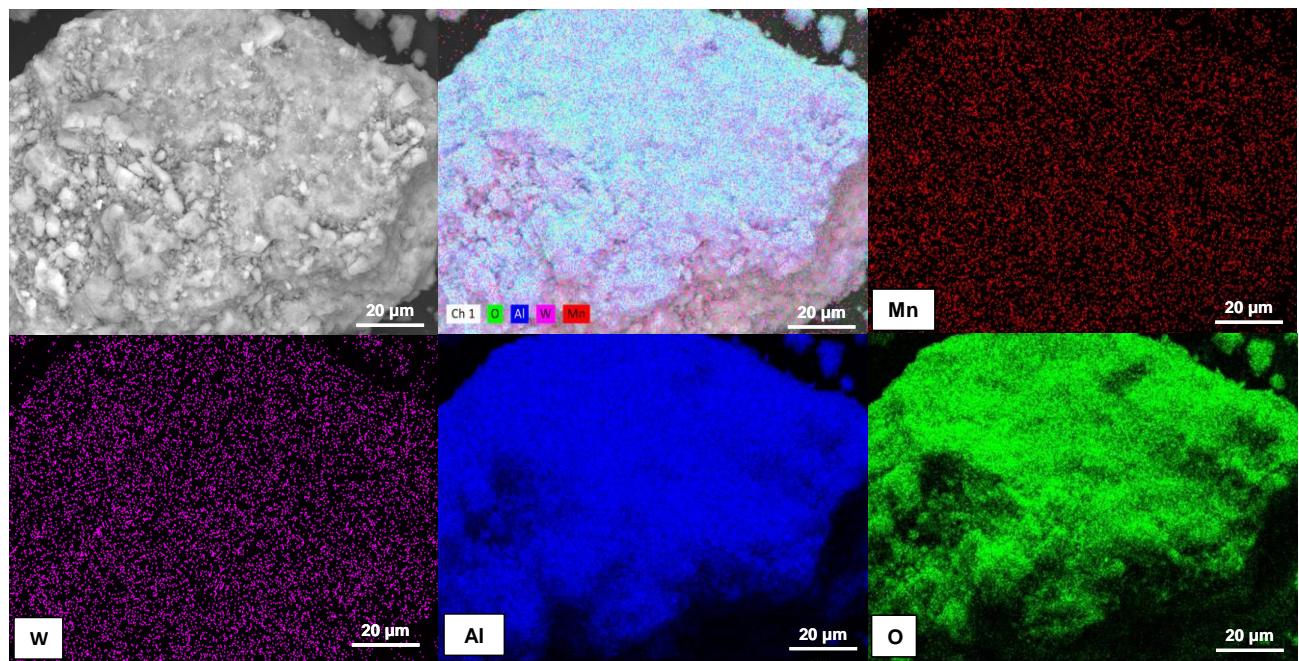
Catalytic performance of samples in ozone decomposition and ozone catalytic oxidation of *n*-C<sub>4</sub>H<sub>10</sub> (OZCO) was studied using fixed-bed flow quartz reactor (id=10mm) operating at atmospheric pressure (Fig S1). The composition of the feed gas contains 100 ppm *n*-C<sub>4</sub>H<sub>10</sub>, 1600 ppm O<sub>3</sub>, 10 vol. % O<sub>2</sub>, balanced with N<sub>2</sub>. Ozone was obtained using a Med ozone YOTA-60-01 ozone generator (Med ozone, Russia). Total flow rate was fixed at 750 mL/min (GHSV = 150 000 h<sup>-1</sup>). The temperature was ranged from RT to 350°C at a heating rate of 5°C/min. Ozone content at the inlet and outlet of the reactor was measured by ozone analyzer Med ozone 254/5 (Med ozone, Russia). Reaction products were analyzed by FTIR gas analyzer “Gasmet” (Temet Instruments DX-4000). The conversion of *n*-C<sub>4</sub>H<sub>10</sub>, was calculated using the follow equation:

$$X = \frac{C_{in} - C_{out}}{C_{in}} \times 100\%$$

where subscripts *in* and *out* are the inlet and outlet concentrations, respectively.



**Figure S1.** Experimental setup



**Figure S2.** Surface morphology and EDS of 1% Mn8%W/Al<sub>2</sub>O<sub>3</sub>