

# Fast and standard selective catalytic reduction in $\text{NH}_3\text{-DeNO}_x$ : pathways discrimination as a key step for the understanding of kinetics

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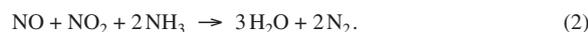
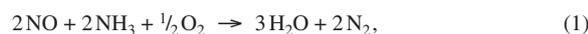
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Two methods for distinguishing the fast and standard selective catalytic reduction (SCR) pathways were proposed, and fast SCR activities of Fe-Beta catalysts containing 0.7, 0.2 and 0.02% Fe were compared.

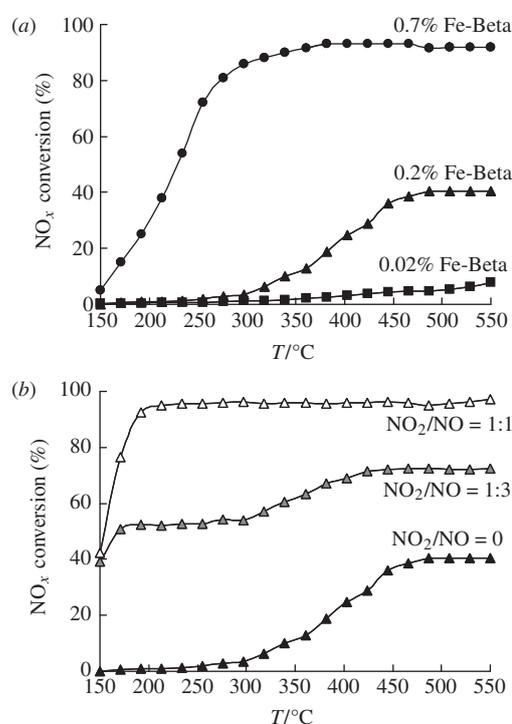
Selective catalytic reduction by ammonia ( $\text{NH}_3\text{-SCR}$ ) is one of the most efficient technologies for removing  $\text{NO}_x$ . However, the efficiency of standard SCR process (1) is insufficient at low temperatures (150–250 °C). A possible solution to this issue is so-called fast SCR reaction (2) known since Kasaoka *et al.*<sup>1(a)</sup> found that the rate of the reaction involving an equimolar NO and  $\text{NO}_2$  feed mixture is much higher than that of standard SCR at a low temperature.



Since the first generation of commercial SCR catalysts for mobile applications were vanadia-based catalysts, the fast SCR reaction over powdered and monolithic  $\text{V}_2\text{O}_5\text{-WO}_3\text{-TiO}_2$  catalysts was extensively investigated.<sup>1</sup> On the other hand, the next generation of  $\text{NH}_3\text{-SCR}$  catalysts are zeolites promoted by transition metals.<sup>2</sup> These catalysts demonstrate favorable  $\text{DeNO}_x$  activity in the standard and, especially, fast SCR reactions. The reactivity, mechanism and kinetics of the fast  $\text{NO}/\text{NO}_2\text{-NH}_3$  SCR reaction over zeolite-based catalysts were studied.<sup>3–5</sup> Sjövall *et al.*<sup>6</sup> developed a transient kinetic model for the fast SCR on a Fe-Beta catalyst; however, they did not take into account the standard SCR activity of  $\text{Fe}^{3+}$  cations<sup>7</sup> and the fact that, in many cases, the fast SCR is an integral part of the overall SCR process. Therefore, this model cannot be used for estimating the quantitative parameters of fast SCR individually. The nature of active sites for fast SCR also remains unclear.

Here, we propose two methods for distinguishing the fast and standard SCR pathways using (1) an under-stoichiometric  $\text{NO}_2/\text{NO}$  mixture (1:3) and (2) ‘ $\text{NO}_2$  slip’ as the criterion of activity. These methods allowed us to compare the efficiency of Fe-Beta catalysts in the fast SCR reaction. Beta zeolite samples with different Fe content were used for evaluation of the role of  $\text{Fe}^{3+}$  cations in the fast SCR process.<sup>†</sup>

Figure 1(a) compares the standard SCR activity of Fe-Beta zeolites with different Fe contents. It is clearly seen that 0.02% Fe-Beta demonstrated negligible activity in the standard SCR, while samples



**Figure 1** (a) Standard SCR performance ( $\text{NO}_2/\text{NO} = 0$ ) of Fe-Beta with different Fe contents; (b) SCR performance of 0.02% Fe-Beta under the standard SCR, under-stoichiometric and stoichiometric fast SCR conditions. Gas mixture: 500 ppm of  $\text{NO}_x$ , 530 ppm of  $\text{NH}_3$ , 10%  $\text{O}_2$  and 6%  $\text{H}_2\text{O}$ .

Catalytic tests were carried out in a fixed-bed flow reactor (inner diameter, 4 mm) at a flow rate of  $300 \text{ ml min}^{-1}$  under GHSV of  $270000 \text{ h}^{-1}$  (0.040 g of zeolite was diluted by silicon carbide). All the activity data was measured in the TPR mode: the temperature was decreased from 550 to 150 °C at a rate of  $2 \text{ K min}^{-1}$ .  $\text{NO}_x$  concentrations (in ppm) were measured on a Gaset FTIR gas analyzer (Temet Instruments DX-4000) at regular intervals of 5 s;  $\text{NO}_x$  conversions were calculated from an average of 10 outlet  $\text{NO}_x$  readings with a temperature step of  $\sim 25$  °C.

The feed gas contained 10 vol%  $\text{O}_2$ , 6 vol%  $\text{H}_2\text{O}$ , 530 ppm of  $\text{NH}_3$ , 500 ppm of  $\text{NO}_x$  (standard SCR: 0 ppm of  $\text{NO}_2$ , 500 ppm of NO); the ‘stoichiometric’ fast SCR 1:1 mixture contained 250 ppm of  $\text{NO}_2$  and 250 ppm of NO; the ‘under-stoichiometric’ fast SCR 1:3 mixture contained 125 ppm of  $\text{NO}_2$  and 375 ppm of NO, balanced with  $\text{N}_2$ . All reactor lines were heated to prevent water vapor condensation and ammonium nitrate deposition.

<sup>†</sup> The commercial samples of 0.2 wt% Fe and 0.7 wt% Fe-Beta were used. The 0.02% Fe-Beta sample was synthesized using Fe-free precursors. All catalysts were calcined in air at 550 °C for 4 h; then, they were pressed, crushed and sieved to yield samples with a particle size of 0.2–0.4 mm. Iron concentrations in the samples were determined by ICP-AES.

with higher Fe loadings provided reasonable  $\text{NO}_x$  conversions. Thus, the higher was the Fe content, the better standard SCR performance of the catalysts was observed. These results are in a good agreement with the previous data.<sup>7(b)</sup>

Fe-Beta zeolites also show high activity in fast SCR reaction [50%  $\text{NO}_2$ , Figure 1(b)]. In order to estimate the activities of samples and to reveal the role of  $\text{Fe}^{3+}$  cations in the fast SCR we used (1) an ‘under-stoichiometric’ mixture ( $\text{NO}_2/\text{NO}$ , 1:3) and (2)  $\text{NO}_2$  slip as criteria for fast SCR catalytic activity.

As mentioned above, the 0.2% Fe-Beta sample demonstrated reasonable standard SCR activity [ $\text{NO}_2/\text{NO}$ , 0:1, Figure 1(b)] at 300–550 °C due to residual  $\text{Fe}^{3+}$  cations; however, at lower temperatures (150–300 °C), the activity was negligible. When an ‘under-stoichiometric’ ( $\text{NO}_2/\text{NO}$ , 1:3) mixture was supplied, the fast SCR and standard pathways can be easily discriminated.

(1) Within a temperature range below 300 °C, the SCR process occurs only through the fast SCR pathway. The  $\text{NO}_x$  conversion does not exceed 50% due to the fast SCR reaction stoichiometry; in other words, the  $\text{NO}_x$  conversion is limited by the  $\text{NO}_2$  concentration in feed gas [equation (1)]. Low conversion below 150–170 °C can be explained by  $\text{NH}_4\text{NO}_3$  formation.<sup>2</sup>

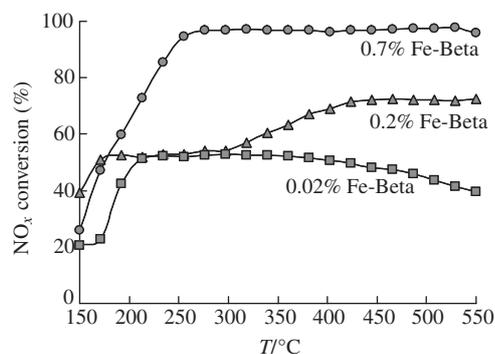
(2) Within a temperature region above 300 °C, the  $\text{NO}_x$  conversion increases proportionally to the contribution of the standard SCR activity of 0.2% Fe-Beta.

Under ‘stoichiometric’ fast SCR conditions [ $\text{NO}_2/\text{NO}$ , 1:1, Figure 1(b)], the  $\text{NO}_x$  conversion on 0.2% Fe-Beta exceeds 95% at  $T_{\text{react}} > 200$  °C, which makes impossible a discrimination of the standard and fast SCR pathways. Thus, only in the case of ‘under-stoichiometric’ fast SCR conditions ( $\text{NO}_2/\text{NO}$ , 1:3), the fast and standard SCR pathways are easily distinguished.

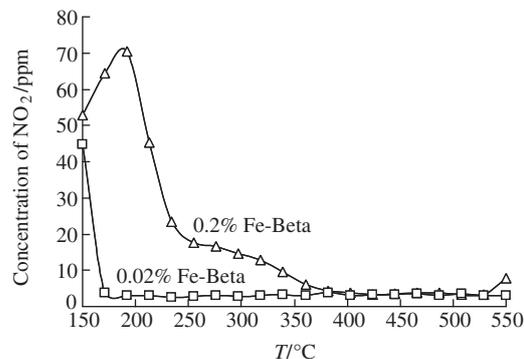
In this study, we used an under-stoichiometric mixture in order to evaluate the role of  $\text{Fe}^{3+}$  cations in the fast SCR process. Figure 2 depicts the temperature dependence of  $\text{NO}_x$  conversion over Fe-Beta catalysts in an under-stoichiometric mixture ( $\text{NO}_2/\text{NO}$ , 1:3). Evidently, it is difficult to differentiate the standard and fast SCR for 0.7% Fe-Beta, since the contribution of standard SCR to the overall process is significant and ~100%  $\text{NO}_x$  conversion is achieved at  $T_{\text{react}} > 200$  °C.

On the other hand, for the catalysts with lower Fe loadings, the standard SCR can be easily distinguished. Over 0.2% Fe-Beta and 0.02% Fe-Beta samples, the  $\text{NO}_x$  conversion does not exceed 50% at  $T_{\text{react}} < 300$  °C because the reaction proceeds only *via* fast SCR pathway (2) and conversion is limited by  $\text{NO}_2$  concentration in accordance with equation (2).

The increase in  $\text{NO}_x$  conversion at  $T_{\text{react}} > 350$  °C over 0.2% Fe-Beta resulted from the contribution of standard SCR. For 0.02% Fe-Beta, the contribution of Standard SCR is negligible, and  $\text{NO}_x$  conversion is limited by only  $\text{NO}_2$  concentration. The marginal decrease in  $\text{NO}_x$  conversion over 0.02% Fe-Beta at  $T_{\text{react}} > 400$  °C, can probably be explained by  $\text{NO}_2$  decomposition.



**Figure 2** Effect of Fe content on the fast SCR performance of Fe-Beta under under-stoichiometric conditions ( $\text{NO}_2/\text{NO} = 1:3$ ). Gas mixture: 125 ppm of  $\text{NO}_2$ , 375 ppm of  $\text{NO}$ , 530 ppm of  $\text{NH}_3$ , 10%  $\text{O}_2$  and 6%  $\text{H}_2\text{O}$ .



**Figure 3** Concentration of  $\text{NO}_2$  in the outlet gas during the fast SCR over Fe-Beta with different Fe contents under stoichiometric conditions ( $\text{NO}_2/\text{NO} = 1:1$ ). Gas mixture: 200 ppm of  $\text{NO}_2$ , 300 ppm of  $\text{NO}$ , 530 ppm of  $\text{NH}_3$ , 10%  $\text{O}_2$  and 6%  $\text{H}_2\text{O}$ .

It is informative to compare  $\text{NO}_x$  conversions over 0.2% Fe-Beta and 0.02% Fe-Beta catalysts at  $T_{\text{react}} = 170$ – $200$  °C where only the fast SCR takes place. This comparison clearly indicates that 0.2% Fe-Beta is evidently more active than 0.02% Fe-Beta indicating a positive role of  $\text{Fe}^{3+}$  cations in the fast SCR. The data are consistent with the recent results on the decisive role of  $\text{Fe}^{3+}$  species in ZSM-5 cationic positions in both standard and fast SCR processes.<sup>8,9</sup>

Differences in the fast SCR activities of Fe-Beta catalysts with low Fe loadings (0.2 and 0.02 wt% Fe) were additionally evaluated using residual  $\text{NO}_2$  concentrations in the reaction product (*i.e.*,  $\text{NO}_2$  slip) as a criterion. Figure 3 shows the temperature dependence of  $\text{NO}_2$  slip in the course of the fast SCR (under stoichiometric conditions of  $\text{NO}_2/\text{NO}$  ratio ~1:1).

The difference in  $\text{NO}_2$  slips is evident: 0.2% Fe-Beta is significantly more active than 0.02% Fe-Beta in a temperature range of 170–350 °C since an  $\text{NO}_2$  slip is observed only at  $T_{\text{react}} < 170$  °C over 0.2% Fe-Beta. These data suggest a positive role of  $\text{Fe}^{3+}$  species in the fast SCR reaction.

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